

QDMC Using a Reduced-Order SVD-KL Model of a Distributed Parameter System

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Objectives

- ♠ **Develop a finite reduced-order model of DPS using plant data**
- ♠ **Demonstrate the reduction method on a nonlinear reaction system**
- ♠ **Develop a Quadratic Dynamic Model-based Controller (QDMC) using SVD-KL model**
- ♠ **Demonstrate the QDMC controller development on a nonlinear reaction system**

Input/Output representation

- ♠ Input/output characteristics of nonlinear systems may be represented by Volterra series.
- ♠ The Volterra series kernels can be identified analytically when the exact mathematical description of the process is known.
- ♠ Otherwise kernel must be identified from the data.

For general nonlinear systems: linear models

First-order Volterra model:

$$y(t) = w^0(t, \mathbf{x}) + \int_0^t w(\tau)u(t - \tau)d\tau$$

State space (linear time-invariant) model:

$$y(t) = Ce^{At}\mathbf{x}^0 + \int_0^t Ce^{A(t-\tau)}Bu(t - \tau)d\tau$$

Kernels from the data

$$\text{Inputs } \Delta u(z, t) = \sum_{r=1}^m p_r(z) a_r(t)$$

$$\text{Outputs } y(z, t) = \sum_{r=1}^n q_r(z) b_r(t)$$

Kernel: $k(z, \zeta, \tau)$

Input/Output Model:

$$y(z, t) = \int_0^t \int_{\Omega} k(z, \zeta, \tau) \Delta u(\zeta, t - \tau) d\zeta d\tau$$

$$t_0 \leq t \leq t_f \quad z \in \Omega$$

Methodology

- ♠ **SVD: defines the kernel coefficient matrix**
- ♠ **Galerkin: solves the kernel coefficient matrix**
- ♠ **Input/output Model:
discrete-time, first-order Volterra series
approximation**

SVD of the kernel in spatial direction

$$\mathbf{k}(\mathbf{z}, \zeta, \tau) = \sum_{i=1}^{\infty} w_i(\mathbf{z}, \tau) \sigma_i(\tau) \overline{\nu_i(\zeta, \tau)}$$

$$\nu_i(\zeta, \tau) = \sum_{l=1}^m p_l(\zeta) \nu_{li}(\tau)$$

$$w_i(\mathbf{z}, \tau) = \sum_{k=1}^n q_k(\mathbf{z}) w_{ki}(\tau)$$

$$\mathbf{k}(\mathbf{z}, \zeta, \tau) \simeq \sum_{i=1}^{\min(m,n)} w_i(\mathbf{z}, \tau) \sigma_i(\tau) \overline{\nu_i(\zeta, \tau)}$$

kernel

$$\int_0^t \int_{\Omega} \sum_{r=1}^N \left[\sum_{k=1}^n q_k(\mathbf{z}) w_{kr}(\tau) \sigma_r(\tau) \sum_{l=1}^m \overline{\nu_{lr}(\tau) p_l(\zeta)} \right] \sum_{l=1}^m p_l(\zeta) \mathbf{a}_l(t - \tau) d\zeta d\tau$$

$$\simeq \sum_{l=1}^n \mathbf{q}_l(\mathbf{z}) \mathbf{b}_l(t)$$

Galerkin projection

$$\int_0^t \mathcal{Q} (\mathcal{W}(\tau) \Sigma(\tau) \bar{\mathcal{V}}(\tau)) \mathcal{P} \mathbf{a}(t - \tau) d\tau = \mathcal{Q} \mathbf{b}(t)$$
$$\mathcal{Q} \equiv \int_{\Omega} \mathbf{q}(\zeta) \mathbf{q}^T(\zeta) d\zeta, \quad \mathcal{P} \equiv \int_{\Omega} \mathbf{p}(\zeta) \mathbf{p}^T(\zeta) d\zeta$$
$$\mathcal{W} \equiv \{\mathbf{w}_{kl}(\tau)\}, \quad \mathcal{V} \equiv \{\nu_{rl}(\tau)\}, \quad \Sigma \equiv \text{diag}\{\sigma_l(\tau)\}$$

Kernel: at time kT

$$y(\mathbf{z}, kT) = \int_{\Omega} \sum_{\ell=1}^{\infty} \int_{(\ell-1)T}^{\ell T} \kappa(\mathbf{z}, \zeta, \tau) d\tau \Delta \mathbf{u}_{k-\ell}(\zeta) d\zeta$$
$$\approx \sum_{\ell=1}^N \int_{\Omega} \kappa(\mathbf{z}, \zeta, \ell) \Delta \mathbf{u}_{k-\ell}(\zeta) d\zeta$$

Kernel from data

$$\sum_{\ell=1}^N \mathcal{Q} \left(\mathcal{W}(\ell) \Sigma(\ell) \bar{\mathcal{V}}(\ell) \right) \mathcal{P} \mathbf{a}_{\mathbf{k}-\ell} = \mathcal{Q} \mathbf{b}(\mathbf{k})$$

Open loop tests: I/O data a and b

Input, Output coefficient matrices: A, B

Least-square approach

$$\bar{\mathbf{K}} \equiv \mathbf{B} \mathbf{A}^\dagger$$

$$\mathbf{A} \in m\mathbf{N} \times (\mathbf{P} + 1), \quad \mathbf{B} \in \mathbf{n} \times (\mathbf{P} + 1)$$

$\bar{\mathbf{K}} = \{K(1), \dots, K(N)\}$: **Coefficient matrices**

Coefficient Matrix at ℓ

$$\mathbf{K}(\ell) = \mathcal{Q} \left(\mathcal{W}(\ell) \Sigma(\ell) \bar{\mathcal{V}}(\ell) \right) \mathcal{P} \quad \ell = 1, \dots, \mathbf{N}$$

$$\mathbf{K}(\ell) \in \mathbf{n} \times \mathbf{m}$$

Methodology

- ♠ **Dominant spatial effect of the inputs on the outputs: Karhunen-Loève Expansion**
 - Identify the dominant empirical eigenfunctions (EEFs): functions of spatial variables
- ♠ **Project the SVD kernels onto the dominant EEFs: kernel approximation with dominant spatial behavior**
 $(\hat{\kappa}^{ij}(z, \zeta, t))$
- ♠ **Finite input/output model: function of the dominance captured in the kernel**

Karhunen-Loève Expansion

Spatial correlation function:

$$\mathcal{R}(z, \zeta) = \lim_{T \rightarrow \infty} \frac{1}{T} \int_0^T \nu(z, t) \nu(\zeta, t) dt$$

Eigenvalue(λ_j) / eigenfunction ($\phi_j(z)$) problem

$$\int_0^1 \mathcal{R}(z, \zeta) \phi_j(\zeta) d\zeta = \lambda_j \phi_j(z)$$

Mercer's theorem [Naylor, 1971]

$$\mathcal{R}(z, \zeta) = \sum_{k=1}^{\infty} \lambda_k \phi_k(z) \phi_k(\zeta)$$

Empirical eigenfunction (EEF):

$$\phi_j(z) = \sum_{k=1}^N \alpha_{kj} \nu_k(z) \quad j = 1, \dots$$

Projection

- First few largest eigenvalues represent the dominant behavior.
- The dominant eigenfunctions are the basis functions in an orthogonal projection.

KL expansion to the Dynamic Kernel

$$\hat{\kappa}^{ij}(\mathbf{z}, \zeta, \ell) \simeq \sum_{l=1}^n \phi_1^{ij}(\mathbf{z}, \zeta) \mathcal{T}_1^{ij}(\ell) \quad t_0 \leq t \leq t_f$$
$$\mathcal{T}_1^{ij}(\ell) = \left(\kappa^{ij}(\mathbf{z}, \zeta, t), \phi_1^{ij}(\mathbf{z}, \zeta) \right)$$

i^{th} output:

$$y_i(\mathbf{z}, \mathbf{kT}) \simeq \sum_{\ell=1}^N \sum_{j=1}^M \int_{\Omega} \left[\sum_{l=1}^n \phi_1^{ij}(\mathbf{z}, \zeta) \mathcal{T}_1^{ij}(\ell) \right] \Delta u_{\mathbf{k}-\ell}^j(\zeta) d\zeta$$

Mean value: $\mu^{ij}(\mathbf{z}, \zeta) \quad j = 1, \dots, M, i = 1, \dots, P,$

Summary of SVD-KL procedure

I/O Tests
Collect data

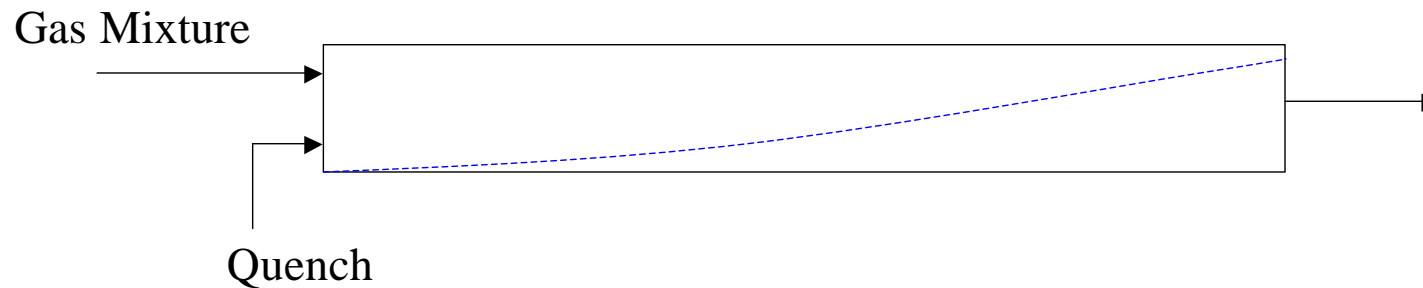
SVD

$$y(z, kT) \approx \sum_{\ell=1}^N \int_{\Omega} \kappa(z, \zeta, \ell) \Delta u_{k-\ell}(\zeta) d\zeta$$

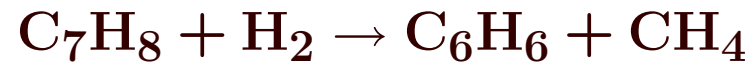
KL expansion

$$y_i(z, kT) \simeq \sum_{\ell=1}^N \sum_{j=1}^M \int_{\Omega} \left[\sum_{l=1}^n \phi_l^{ij}(z, \zeta) \mathcal{T}_l^{ij}(\ell) \right] \Delta u_{k-\ell}^j(\zeta) d\zeta$$

Hydro-dealkylation of Toluene (HDA)



Two reactions are known to occur,



Reactions are exothermic

Temperature between $1150^\circ\text{F} \leq T \leq 1300^\circ\text{F}$

Pressure $500 \text{ psia} \pm 10\%$

Five temperature measurements

Concentration measurement at the exit of the reactor

Quench injection

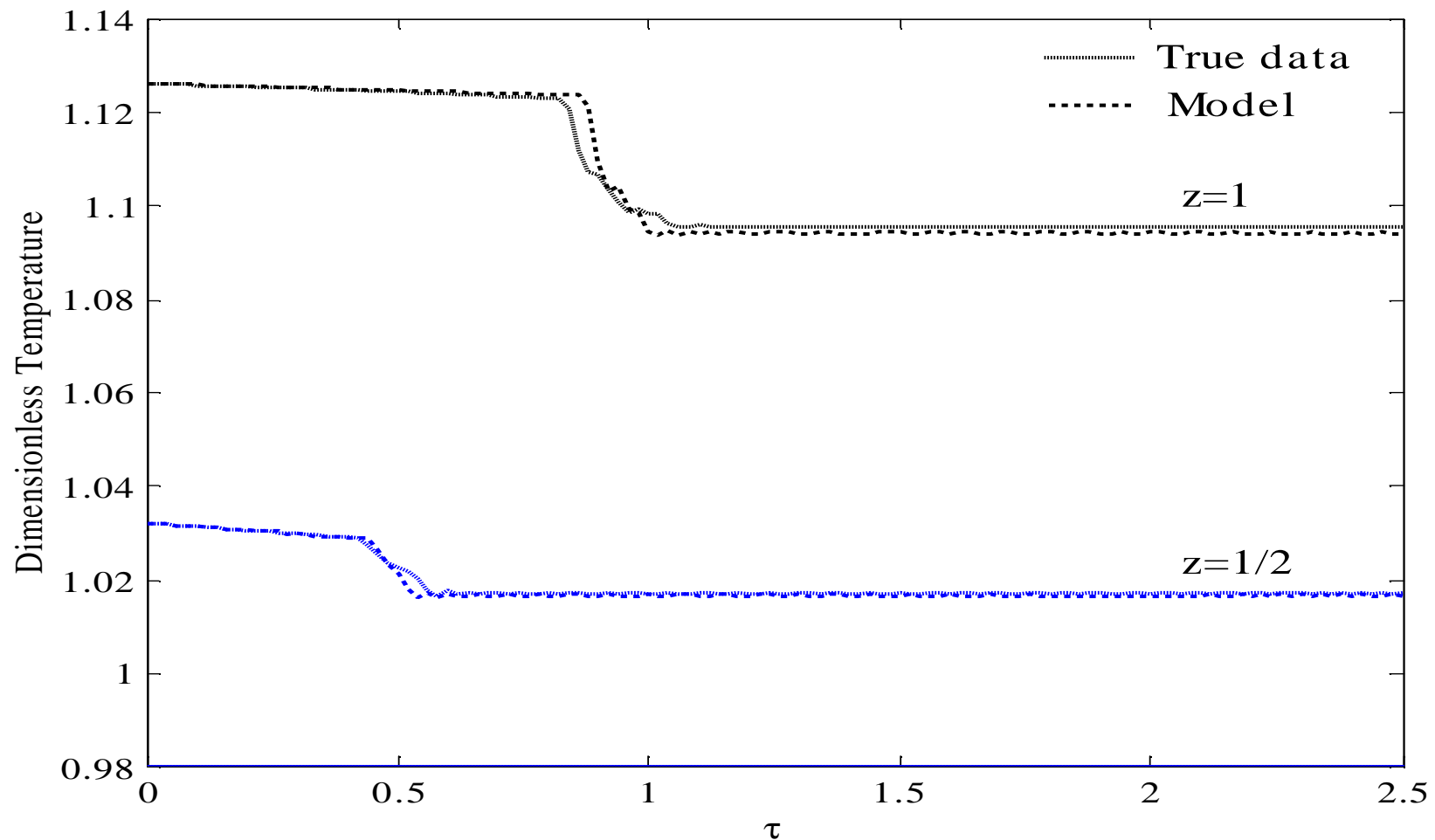
Model of the HDA process

$$\begin{aligned}
 \frac{\partial \xi_1}{\partial \tau} &= -\nu \left[\frac{\partial \xi_1}{\partial \tau_1} + \frac{\xi_1}{\theta} \frac{\partial \theta}{\partial \tau_1} \right] - \xi_1 \xi_2^{0.5} \theta^{1.5} e^{\gamma_1 \frac{\theta-1}{\theta}} \\
 \frac{\partial \xi_2}{\partial \tau} &= -\nu \left[\frac{\partial \xi_2}{\partial \tau_1} + \frac{\xi_2}{\theta} \frac{\partial \theta}{\partial \tau_1} \right] - \xi_1 \xi_2^{0.5} \theta^{1.5} e^{\gamma_1 \frac{\theta-1}{\theta}} + \kappa_2 (\xi_3 \theta)^2 e^{\gamma_2 \frac{\theta-1}{\theta}} - \kappa_3 \xi_2 \xi_5 \theta^2 e^{\gamma_3 \frac{\theta-1}{\theta}} \\
 \frac{\partial \xi_3}{\partial \tau} &= -\nu \left[\frac{\partial x_3}{\partial \tau_1} + \frac{\xi_3}{\theta} \frac{\partial \theta}{\partial \tau_1} \right] + \xi_1 \xi_2^{0.5} \theta^{1.5} e^{\gamma_1 \frac{\theta-1}{\theta}} - 2\kappa_2 (\xi_3 \theta)^2 e^{\gamma_2 \frac{\theta-1}{\theta}} + 2\kappa_3 \xi_2 \xi_5 \theta^2 e^{\gamma_3 \frac{\theta-1}{\theta}} \\
 \frac{\partial \xi_4}{\partial \tau} &= -\nu \left[\frac{\partial \xi_4}{\partial \tau_1} + \frac{\xi_4}{\theta} \frac{\partial \theta}{\partial \tau_1} \right] + \xi_1 \xi_2^{0.5} \theta^{1.5} e^{\gamma_1 \frac{\theta-1}{\theta}} \\
 \frac{\partial \xi_5}{\partial \tau} &= -\nu \left[\frac{\partial \xi_5}{\partial \tau_1} + \frac{\xi_5}{\theta} \frac{\partial \theta}{\partial \tau_1} \right] + \kappa_2 (\xi_3 \theta)^2 e^{\gamma_2 \frac{\theta-1}{\theta}} - \kappa_3 \xi_2 \xi_5 \theta^2 e^{\gamma_3 \frac{\theta-1}{\theta}} \\
 \frac{\partial \theta}{\partial \tau} &= \frac{1}{\zeta} \left(H_{r1} \frac{\partial \xi_1}{\partial \tau} - H_{r2} \frac{\partial \xi_5}{\partial \tau} - \nu \left(\zeta \frac{\partial \theta}{\partial \tau_1} - H_{r1} \frac{\partial \xi_1}{\partial \tau_1} + H_{r2} \frac{\partial \xi_5}{\partial \tau_1} \right) - F_{Bm} \zeta_B \right) \\
 z = 0 & \quad \begin{cases} \xi_j = \xi_j(t = 0) & j = 1, \dots, n_c \\ \theta = \theta(t = 0) \end{cases} & z = 1 & \quad \begin{cases} \frac{\partial \xi_j}{\partial z} = 0 & j = 1, \dots, n_c \\ \frac{\partial \theta}{\partial z} = 0 \end{cases}
 \end{aligned}$$

Model validation at ideal conditions

Temperature

SVD-KL: dashed line, True solution: solid line

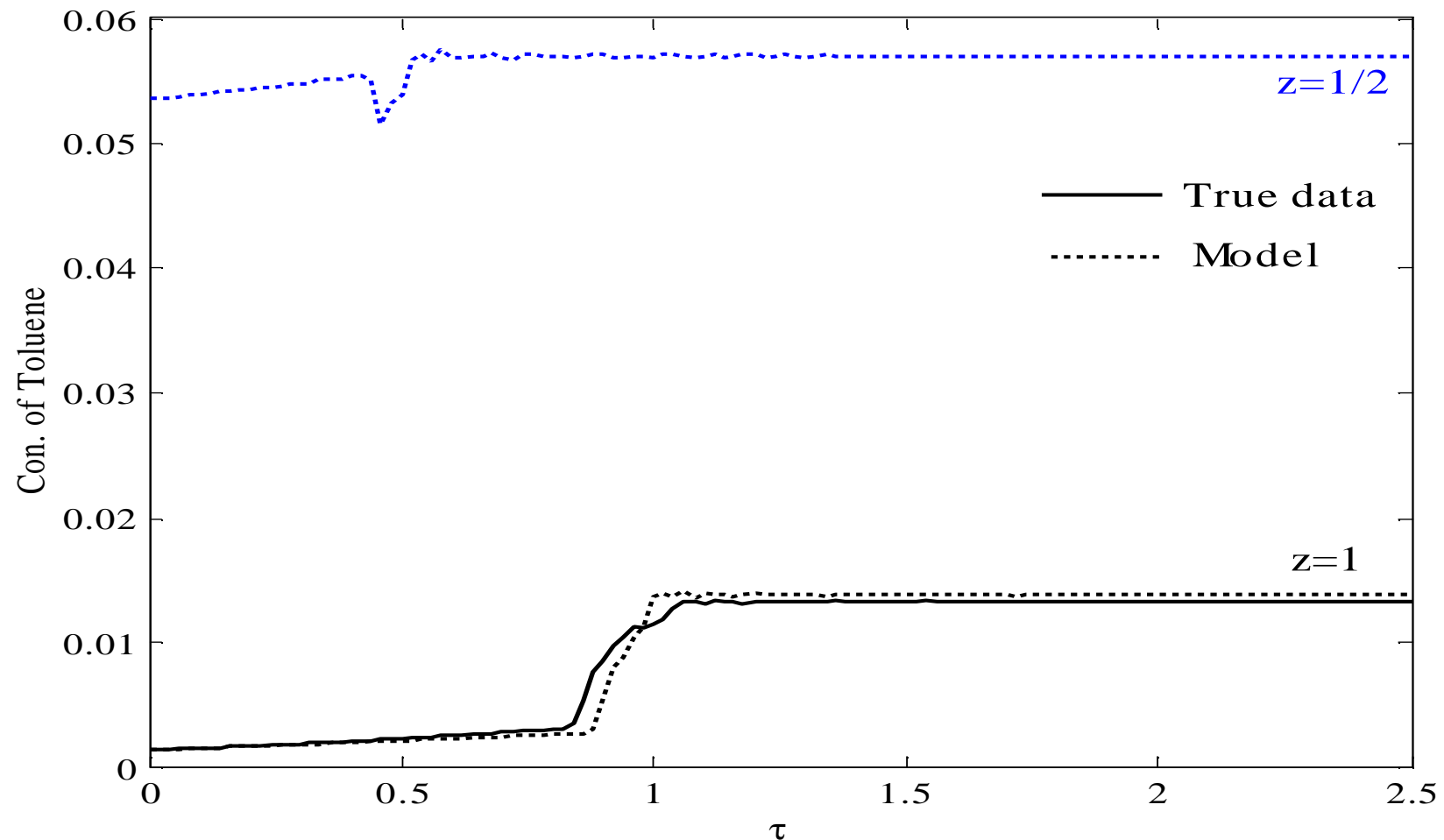


At $z=1$, time averaged error = 0.15%

Model validation at ideal conditions

Concentration of Toluene

SVD-KL: dashed line, True solution: solid line



At $z=1$, time averaged error = 5.25%

Controller Design

- ♠ Quadratic Dynamic Matrix Controller (QDMC)
- ♠ Model: Reduced-order SVD-KL
- ♠ Constraints
- ♠ Disturbance rejection:
 - unmeasured feed temperature disturbance
 - unmeasured feed toluene concentration
 - measured feed flow rate disturbance
- ♠ Comparison with other models
 - Lumped model (reactor modelled as one CSTR)
 - QDMC design
 - NLMPC on nonlinear CSTR model
 - Linearize ODEs at each sample point kT
 - Linearize ODEs - use one linear model

Quadratic DMC: Minimize Quadratic objective

$$\min_{U(k)} E = \frac{1}{2} [y^*(k) - \hat{y}_i(k + \ell | k)]^T \Gamma^T \Gamma [y^*(k) - \hat{y}_i(k + \ell | k)] + \frac{1}{2} U(k)^T \Lambda^T \Lambda U(k)$$

subject to:

$$\hat{y}_i(k + \ell | k) = y_{i0} + \overbrace{\sum_{r=\ell+1}^k k_{ij}^r \Delta u_j(k + \ell - r)}^{\text{past}} + \overbrace{\sum_{r=1}^{\ell} k_{ij}^r \Delta u_j(k + \ell - r)}^{\text{future}} + d(k + \ell | k)$$

Solve QP problem:

$$\min_{U(k)} F = \frac{1}{2} U(k)^T H U(k) - g(k + \ell)^T U(k)$$

$$\text{s.t. } y_i^{\min} \leq y_i \leq y_i^{\max}$$

$$U^{\min} \leq U(k) \leq U^{\max}$$

H : Hessian

$g(e(k + \ell))$: gradient in the direction of U

Closed-loop stability:

Lemma 1 (Unconstrained case) If the eigenvalue spectrum of the matrix

$$\begin{bmatrix} -A_1 I_u H^{-1} A^T w_y K_y + \alpha I_{n_y} & A_1 I_u H^{-1} A^T w_y A_u - \alpha A_1 + A_2 \\ -I_u H^{-1} A^T w_y K_y & I_u H^{-1} A^T w_y A_u \end{bmatrix}$$

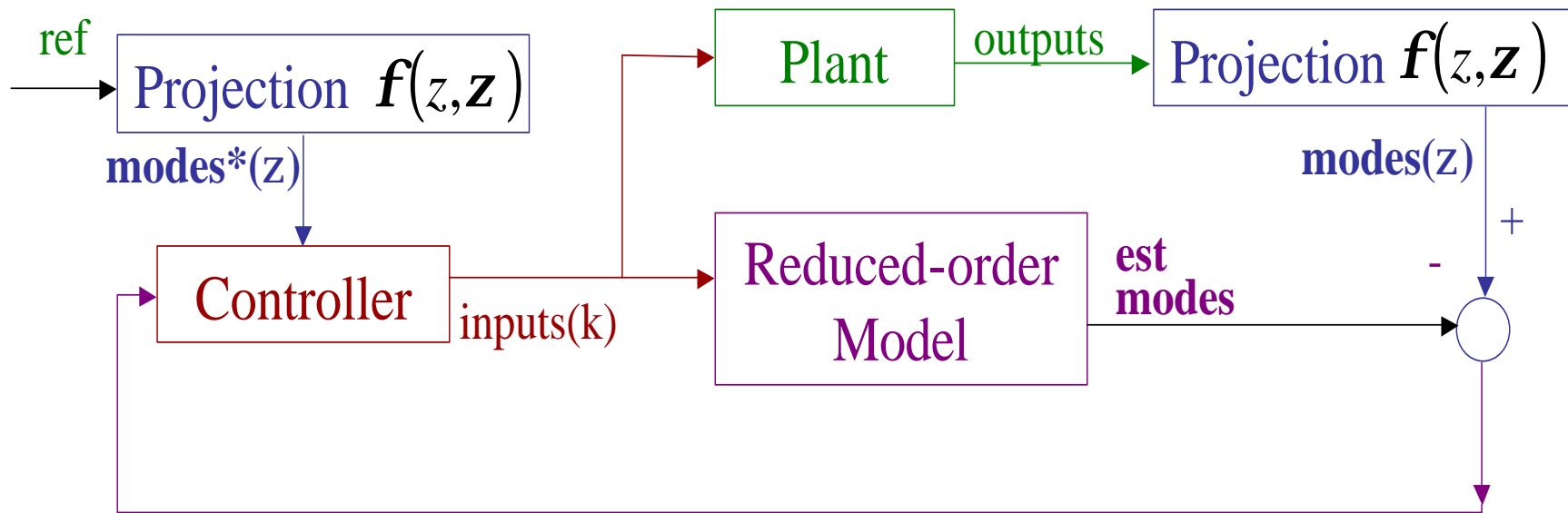
is such that, the largest eigenvalue is less than one, $\max |\lambda_i| < 1$ then the unconstrained system will be closed-loop asymptotically stable.

Lemma 2 (Constrained case) For all the possible active constraints combination, if the eigenvalue spectrum of matrix

$$\begin{bmatrix} -A_1 I_u K_u K_y + \alpha I_{n_y} & A_1 I_u K_u A_u - \alpha A_1 + A_2 \\ -I_u K_u K_y & I_u K_u A_u \end{bmatrix}$$

has $\max |\lambda_i| < 1$ then the closed-loop system is asymptotically stable.

Control Strategy



$$\text{Input}(\mathbf{k}) = \hat{u}_k(\zeta)$$

Modes are functions of ζ

QDMC design

QDMC/SVDKL model:

Control horizon $M = 5$

Weight matrices: $\Gamma = 1$ and $\Lambda = 40$

QDMC/linear CSTR model:

Control horizon $M = 5$

Weight matrices: $\Gamma = 1$ and $\Lambda = 40$

QDMC/nominal linear CSTR model:

Control horizon $M = 5$

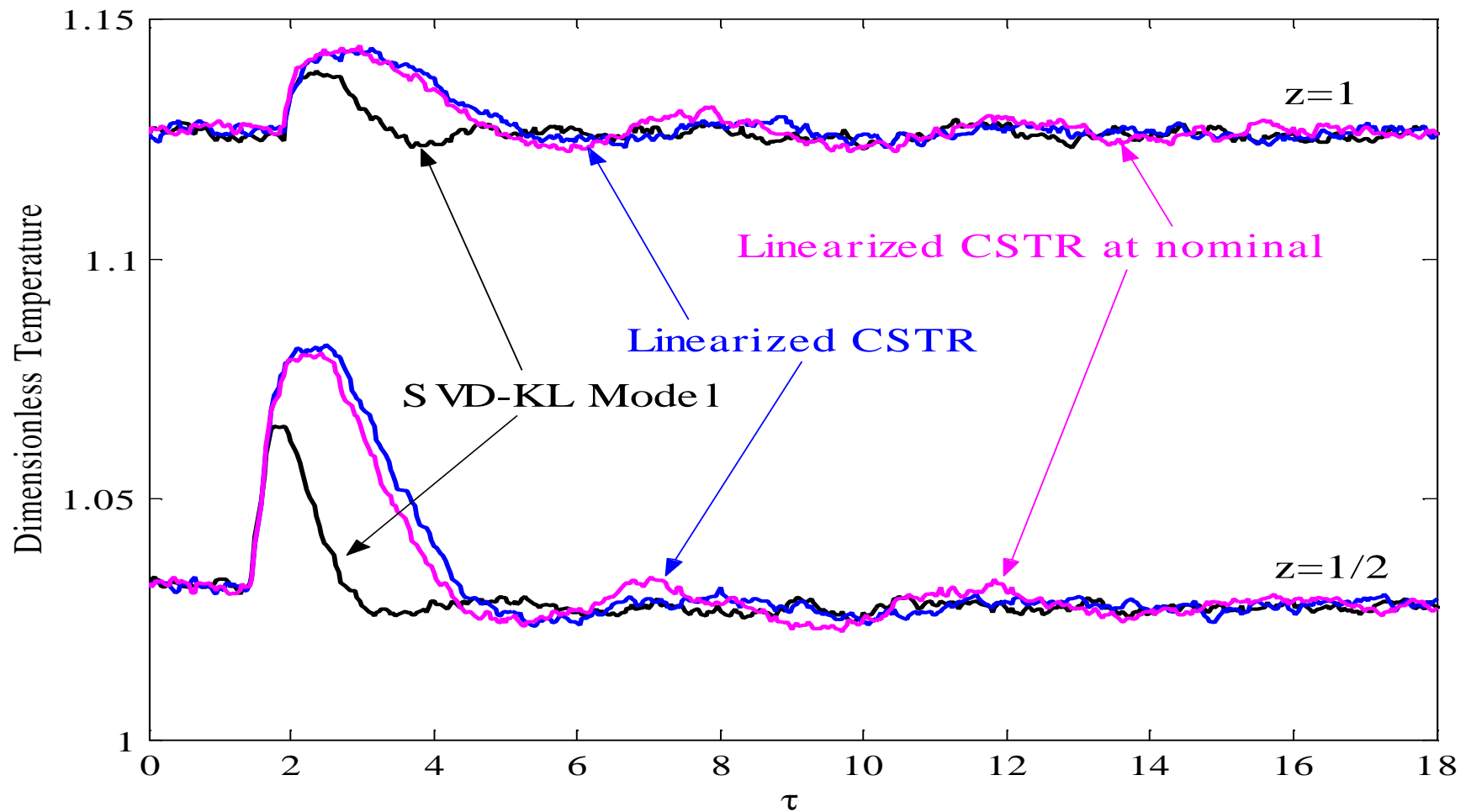
Weight matrices: $\Gamma = 1$ and $\Lambda = 40$

Closed-loop performance

Unmeasured disturbance: Feed temperature (+5%)

Unmeasured disturbance: Feed Toluene concentration (+5%)

Temperature response

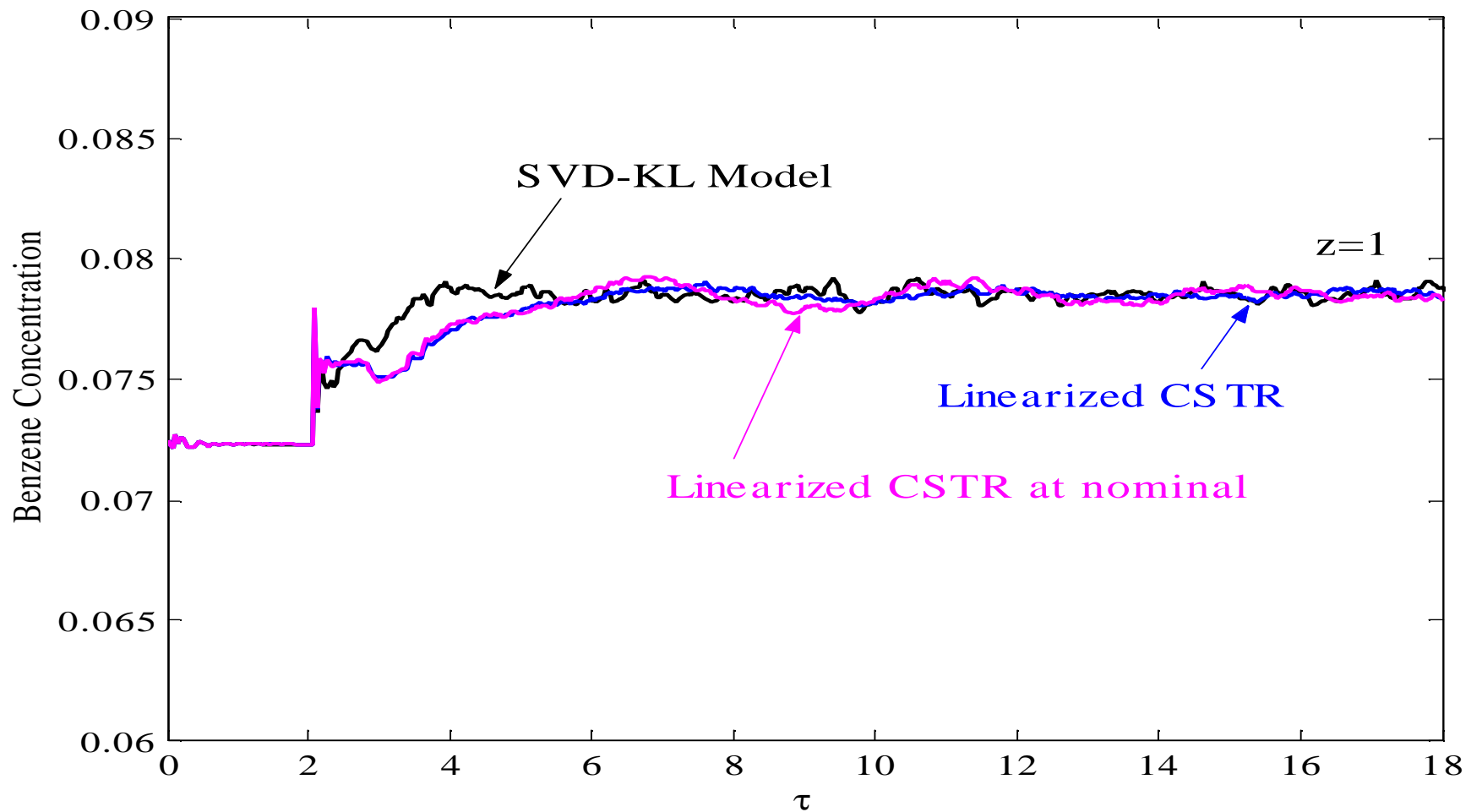


Closed-loop performance

Unmeasured disturbance: Feed temperature (+5%)

Unmeasured disturbance: Feed Toluene concentration (+5%)

Benzene concentration

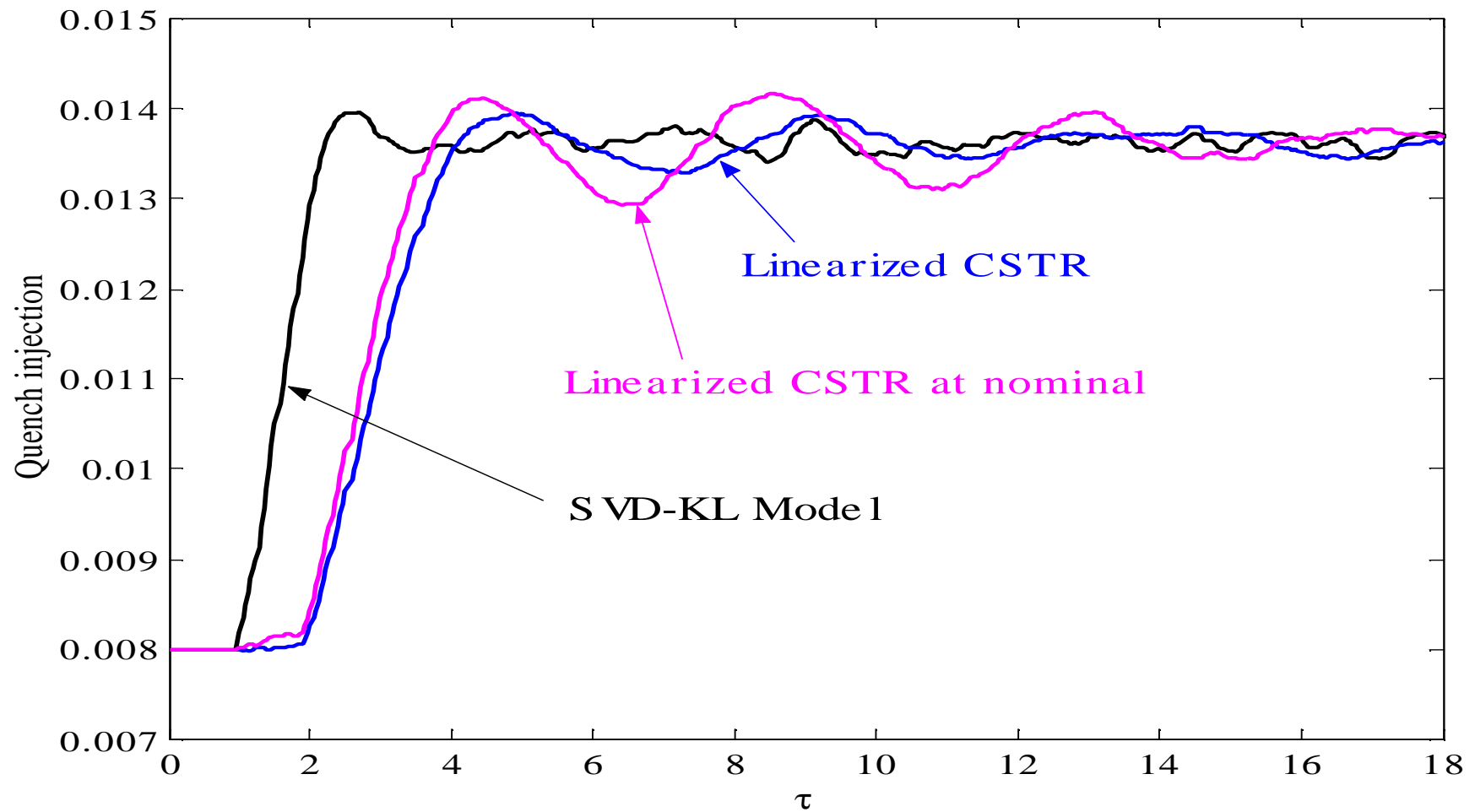


Closed-loop performance

Unmeasured disturbance: Feed temperature (+5%)

Unmeasured disturbance: Feed Toluene concentration (+5%)

Quench

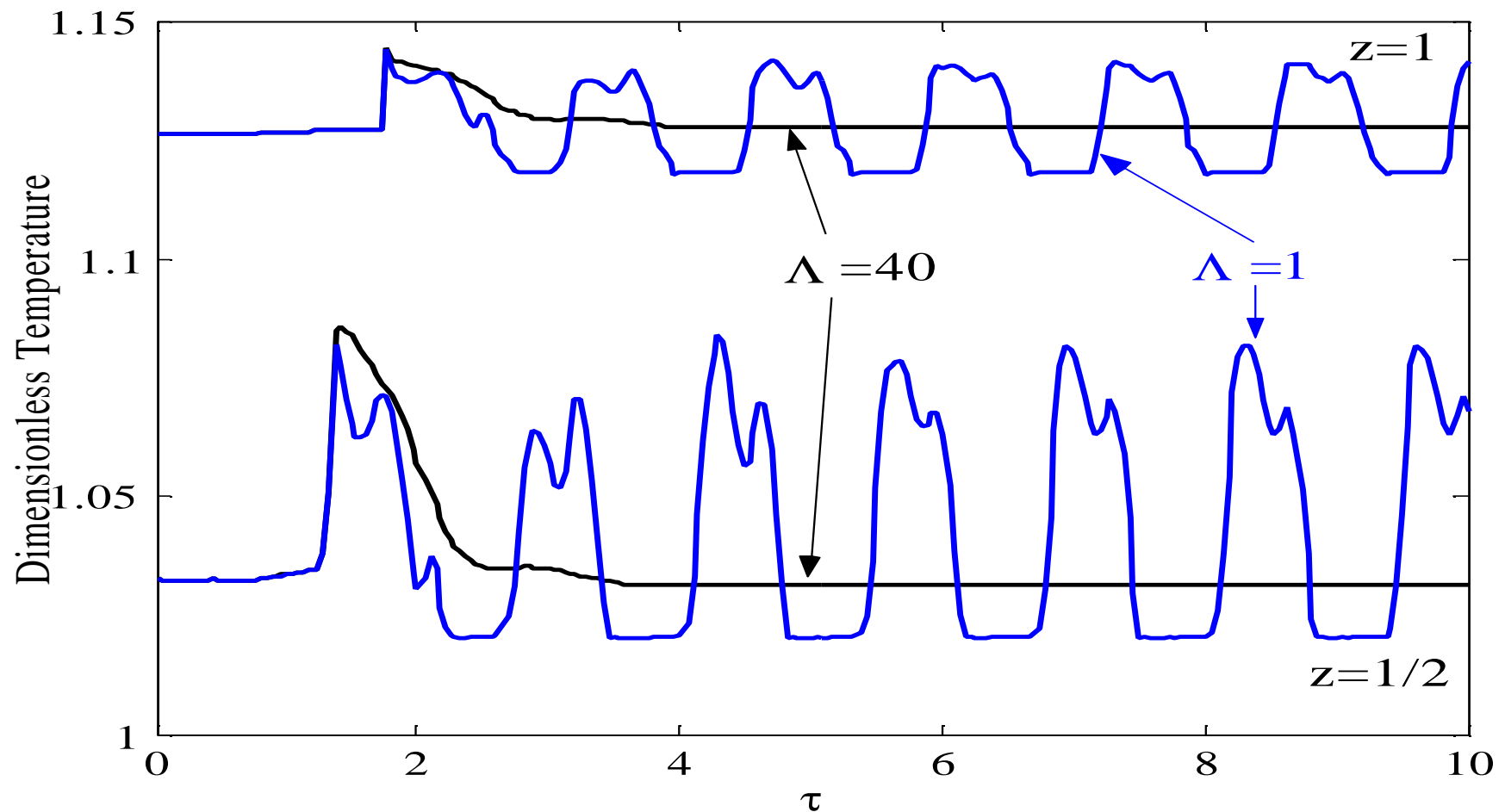


Closed-loop performance

Unmeasured disturbance: Feed temperature (+5%)

Measured disturbance: Feed Flow rate (-3%)

Temperature response

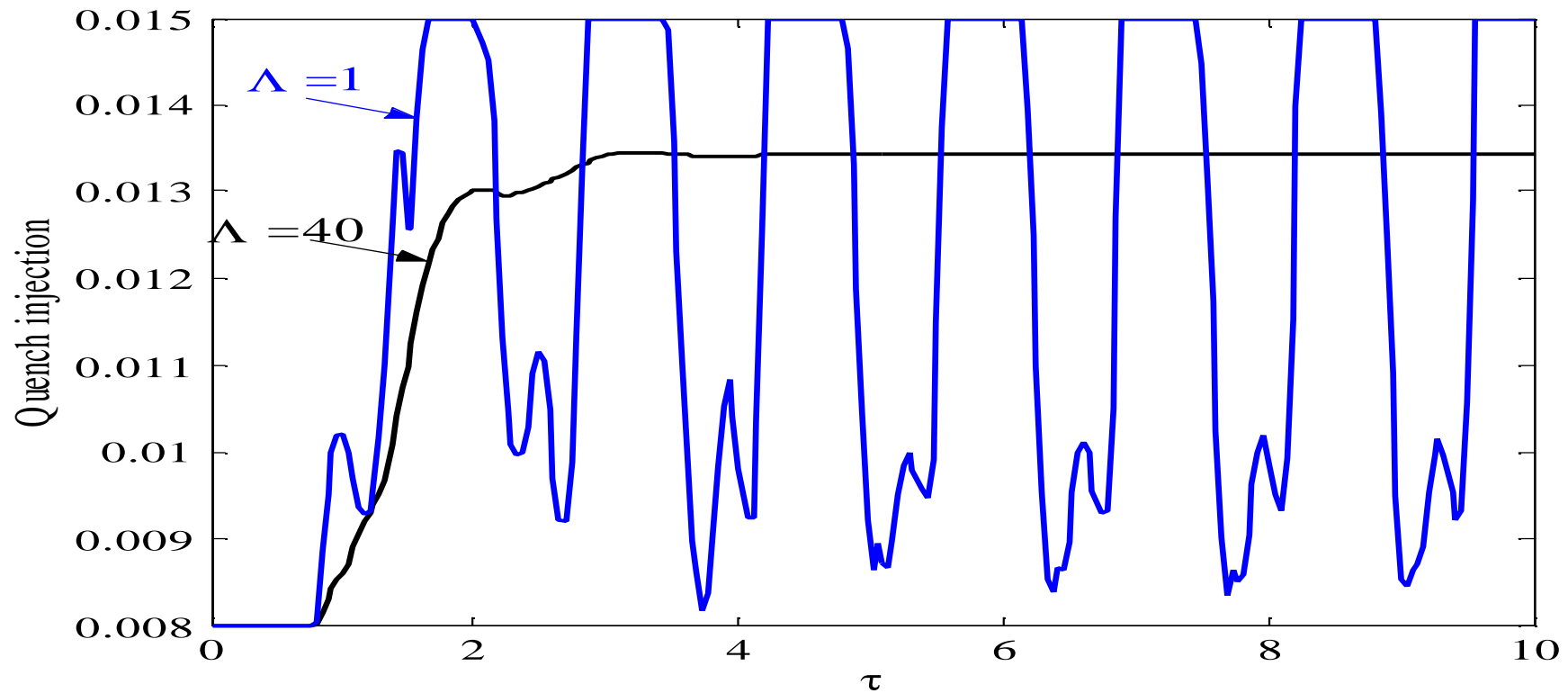


Closed-loop performance

Unmeasured disturbance: Feed temperature (+5%)

Measured disturbance: Feed Flow rate (-3%)

Quench



$$\Lambda = 1 \quad |\lambda|_{max} = 1.2015 \quad \Lambda = 5 \quad |\lambda|_{max} = 1.0165$$

$$\Lambda = 10 \quad |\lambda|_{max} = 1.0011 \quad \Lambda = 40 \quad |\lambda|_{max} = 0.9015$$

Summary

- SVD-KL method yields a finite dimension input-output model that captures the dominant behavior.
- The resulting ij^{th} kernel function contains information of how the j^{th} input acts on the i^{th} output.
- Model-based controller (QDMC) based on the SVD-KL model can be designed.
 - HDA reactor system: nonlinear hyperbolic PDEs
 - Concentration measurement is limited to the exit of the reactor.
 - Satisfactory performance: measured and unmeasured disturbances.
- A sufficient condition for closed-loop stability.

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